



The Numerical Study of Effects of Soret, Dufour and Viscous Dissipation Parameters on Steady MHD Casson Fluid Flow through non-Darcy Porous Media

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Author's contribution

The sole author designed, analyzed and interpreted and prepared the manuscript.

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ABSTRACT

In the present paper the numerical study of effects of Soret, Dufour and viscous dissipation parameters on steady MHD Casson fluid flow through non-Darcy porous medium is explored. By suitable similarity transformations, the governing boundary layer equations are transformed to ordinary differential equations. The method, the numerical computation with *bvp4c*, a MATLAB program, is applied to solve these equations. The effects of magnetic parameter, Soret parameter, Dufour parameter, Prandtl number, Schmidt number, Eckert number, and Casson parameter on velocity, heat transfer, and concentration profiles, Skin- friction, local Nusselt number and local Sherwood number are computed and discussed numerically and presented through tables and graphs.

Keywords: Magnetohydrodynamics; Casson fluid; magnetic parameter; Soret number; Dufour number.

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NOMENCLATURE AND SI UNITS

μ	: Dynamic viscosity ($\text{kgm}^{-2}\text{s}^{-1}$)
ν	: Kinematic viscosity (m^2s^{-1})
B	: Magnetic field ($\text{N}/(\text{mA})$)
H	: Convective heat transfer coefficient ($\text{W}/\text{m}^2\text{K}$)
c	: Specific heat (J/kgK)
D	: Mass diffusivity (m^2s^{-1})
G	: Acceleration due to gravity (ms^{-2})
K	: Thermal conductivity ($\text{Wm}^{-1}\text{K}^{-1}$)
M	: Mass kg
V	: Volume m^3
ρ	: Density kg/m^3
t	: Time (s)
u	: Horizontal component of velocity (m/s)
v	: Vertical component of velocity (m/s)
T	: Temperature of fluid (K)
β	: Thermal expansion coefficient (K^{-1})
M	: Magnetic parameter
N	: Stretching index parameter
Nu	: Local Nusselt number
Pr	: Prandtl number Prandtl number
Re	: Local Reynold number
Sc	: Smidth number
Sh	: Local Sherwood number
C	: Concentration of fluid
Gr_T	: Thermal Grashof number
C_p	: Specific heat at constant pressure
Gr_c	: Mass (concentration) Grashof number
X	: Distance along the plate distance along the plate
α	: Thermal diffusivity
η	: Similarity variable
x, y	: Cartesian coordinates
θ	: Dimensionless temperature
ψ	: Dimensionless stream function

1. INTRODUCTION

Many natural, industrial as well as biological fluids (such as mud, condensed milk, glues, lubricating greases, paints, sugar solution, shampoos and tomato paste, polymers, liquid detergents, blood, fruit juices etc.) change their viscosity or flow behaviour under stress; and thus deviate from the classical Newton's law of viscosity. Different models of non-Newtonian fluids based on their diverse flow behaviours have been proposed by the researchers.

The rheological model was introduced originally by Casson [1] in his research on a flow equation for pigment oil-suspension of printing ink. Bird et al. [2] investigated the rheology and flow of

visco-plastic materials. He reported that Casson model constitutes a plastic fluid model which exhibits shear thinning characteristics, yield stress, and high shear viscosity. Casson fluid behaves as solid when the shear stress is less than the yield stress and it starts to deform when shear stress becomes greater than the yield stress.

The fundamental analysis of the flow field of non-Newtonian fluids in a boundary layer adjacent to a stretching sheet or an extended surface is very important and is an essential part in the study of fluid dynamics, and heat and mass transfer.

Sakiadis [3] studied boundary layer behaviour on continuous solid surfaces: II. The boundary layer on continuous flat surface. Crane [4] studied the flow past a stretching plane. Nield et al. [5] studied convection in porous media.

Mukhopadhyay [6] investigated Casson fluid flow and heat transfer over a nonlinearly stretching surface. Mustafa et al. [7] studied Model for the flow of Casson nanofluid past a non-linearly stretching sheet, considering magnetic field effects. Medikare et al. [8] studied MHD stagnation point flow of a Casson fluid over a nonlinearly stretching sheet with viscous dissipation.

Pramanik [9] studied Casson fluid flow and heat transfer past an exponentially porous stretching surface in presence of thermal radiation. Raju et al. [10] studied heat and mass transfer in magnetohydrodynamic Casson fluid over an exponentially permeable stretching surface. Saidulu et al. [11] studied slip effects on MHD flow of Casson fluid over an exponentially stretching sheet in presence of thermal radiation, heat source/sink and chemical reaction.

Sharada et al. [12] studied MHD mixed convection flow of a Casson fluid over an exponentially stretching surface with the effects of Soret, Dufour, thermal radiation and chemical reaction. Mukhopadhyay et al [13] studied exact solutions for the flow of Casson fluid over a stretching surface with transpiration and heat transfer effects. Hayat et al. [14] investigated Soret and Dufour effects on magnetohydrodynamic (MHD) flow of Casson fluid.

Mahdy [15] studied heat transfer and flow of a Casson fluid due to a stretching cylinder with the Soret and Dufour effects. Animasaun [16] studied

effects of thermophoresis, variable viscosity and thermal conductivity on free convective heat and mass transfer of non-Darcian MHD dissipative Casson fluid flow with suction and n th order of chemical reaction.

Ullah et al. [17] investigated Effects of slip condition and Newtonian heating on MHD flow of Casson fluid over a nonlinearly stretching sheet saturated in a porous medium.

Some recent studies concerning the flow, heat and mass transfer analysis of Casson fluid can be found in Refs [18–58].

We consider (1) non-Darcy porous medium, (2) thermo –diffusion(Dufour term) term in energy equation, (3) mass equations, (4) diffusion -thermo term (Soret term) in the mass equation and (5) nonlinear surface (6), velocity slip factor, thermal slip factor, and mass slip factor in boundary conditions of velocity, temperature, and concentration respectively. In the study of references as mentioned above, these terms, simultaneously in one problem, are not investigated with the flow over nonlinear surface.

The present work is the extension of Ullah et al. [17] work, by considering above terms.

It deals with the numerical study of effects of Soret Dufour and viscous dissipation parameters on steady MHD Casson fluid flow through non-Darcy porous medium.

2. MATHEMATICAL FORMULATION OF THE PROBLEM

In the formulation of the problem we consider following assumptions. Casson fluid is incompressible and electrically conducting. Flow is steady, laminar and two dimensional over a nonlinearly stretching sheet. Flow region is in non-Darcy porous medium. It is under the influence of transverse magnetic field B . The sheet is stretched nonlinearly along the x -axis (i.e. $y=0$) with velocity $u_w(x) = cx^n$; origin is taken as fixed and the fluid flow is confined to $y>0$. Here c is constant and $n(n \geq 0)$ is the nonlinear stretching sheet parameter; $n=1$ represents the linear sheet case and $n \neq 1$ is for nonlinear case. The magnetic Reynolds number of the flow is taken to be small enough so that induced magnetic field is assumed to be negligible in comparison with applied magnetic

field so that $B = (0, B(x), 0)$, where $B(x)$ is the applied magnetic field acting normal to the plate and varies in strength as a function of x . The flow is assumed to be in the x -direction which is taken along the plate and y -axis is normal to it. There is a constant suction/injection velocity v_w normal to the plate.

Under these assumptions the rheological equation for incompressible flow of Casson fluid is given by (Sharada et al. [12], Mukhopadhyay et al. [13])

$$\tau_{ij} = \begin{cases} 2(\mu_B + p_y / \sqrt{2\pi})e_{ij} & \pi > \pi_c, \\ 2(\mu_B + p_y / \sqrt{2\pi_c})e_{ij} & \pi < \pi_c \end{cases}$$

where $\pi = e_{ij} e_{ij}$ and e_{ij} is the (i, j) -th component of the deformation rate, π is the product of the components of deformation, π_c is critical value of the product based on the non-Newtonian model, μ_B is the plastic dynamic viscosity of the non-Newtonian fluid, and p_y is the yield stress of the fluid. The viscosity and thermal conductivity of the fluid are assumed to be constant. There is thermo-diffusion effect as well as diffusion-thermo effect. The pressure gradient, body forces and Joule heating are neglected compared with the effect of viscous dissipation. The temperature and concentration of the stretching surface are always greater than their free stream values. The flow configuration and the coordinate system are shown in Fig. 1.

Under the above assumptions and using Boussinesq approximation, boundary layer equations for flow with heat and mass transfer in Casson fluid are given by the following.

The continuity equation:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \tag{1}$$

The momentum equation:

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \nu \left(1 + \frac{1}{\beta} \right) \frac{\partial^2 u}{\partial y^2} + g\beta_T(T - T_\infty) + g\beta_C(C - C_\infty) - \frac{\sigma B^2(x)}{\rho} u - \frac{\nu}{K} u - \frac{b}{\sqrt{K}} u^2 \tag{2}$$

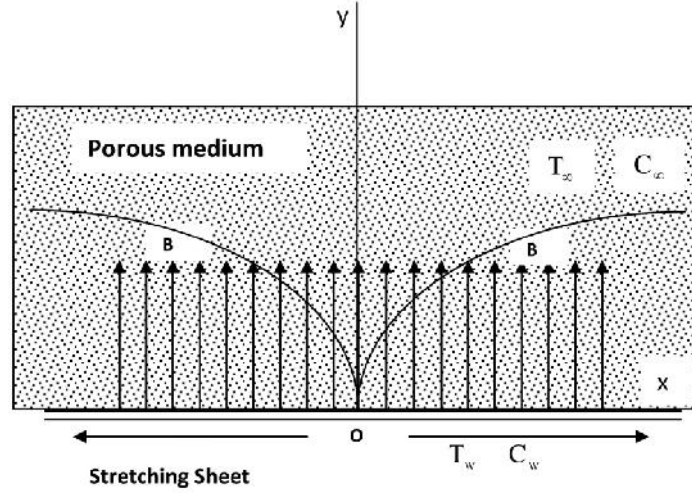


Fig. 1. Physical model and coordinate system

The energy equation:

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y^2} + \left(\frac{D_m K_T}{C_s C_p} \right) \frac{\partial^2 C}{\partial y^2} + \frac{\mu}{\rho C_p} \left(1 + \frac{1}{\beta} \right) \left(\frac{\partial u}{\partial y} \right)^2 \quad (3)$$

The mass equation:

$$u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = D_m \frac{\partial^2 C}{\partial y^2} + \left(\frac{D_m K_T}{T_M} \right) \frac{\partial^2 T}{\partial y^2} \quad (4)$$

where u and v are velocity components along x and y axes, respectively, ρ is fluid density, ν is kinematic viscosity, μ is dynamic viscosity, $\beta = \mu_B \sqrt{2\pi} / p_y$ is the Casson fluid parameter, σ is the electrical conductivity of the fluid and is assumed to be constant, β_T is the coefficient of

thermal expansion, β_C is the coefficient of concentration expansion, T_w is the temperature of the fluid at the stretching sheet, T is the temperature of the fluid within the boundary layer, T_∞ is the temperature of the fluid outside the boundary layer, k is the thermal conductivity of the fluid, C_p is the specific heat at constant pressure p , C_w is the concentration of the fluid at the stretching sheet, C is the concentration of the fluid within the boundary layer, C_∞ is the concentration of the fluid outside the boundary layer, D_M is the chemical molecular diffusivity. Here, g is the acceleration due to gravity. The applied magnetic field is $B = B_0 x^{\frac{n-1}{2}}$, where B_0 is assumed to be constant.

Boundary conditions (Ullah et al. [17]):

$$\begin{aligned} \text{At } y = 0 : u &= cx^n + N_1 \nu \left(1 + \frac{1}{\beta} \right) \frac{\partial u}{\partial y}, \quad v = 0, \quad \frac{\partial T}{\partial y} = -h_s (T - T_w), \quad \frac{\partial C}{\partial y} = -h_c (C - C_w) \\ \text{As } y \rightarrow \infty : u &\rightarrow 0, \quad T \rightarrow T_\infty, \quad C \rightarrow C_\infty. \end{aligned} \quad (5)$$

Here $N_1(x) = N x^{-\frac{n-1}{2}}$ denotes velocity of slip factor; it depends upon x , and $h_s(x) = h_{T0} c x^{\frac{n-1}{2}}$ represents the heat transfer parameter for Newtonian heating or temperature slip factor, and $h_c(x) = h_{c0} c x^{\frac{n-1}{2}}$ is concentration slip factor.

We consider following dimensionless variable to transform the system of equations (2), (3), (4) and (5) into a dimensionless form (Ullah et al. [17]):

$$\psi = \left(\frac{2\nu c}{n+1}\right)^{\frac{1}{2}} x^{\frac{n+1}{2}} f(\eta), \eta = \left(\frac{c(n+1)}{2\nu}\right)^{\frac{1}{2}} x^{\frac{n-1}{2}} y, \theta(\eta) = \frac{(T - T_\infty)}{(T_w - T_\infty)}, \phi(\eta) = \frac{(C - C_\infty)}{(C_w - C_\infty)}, \quad (6)$$

$$u = \frac{\partial \psi}{\partial y}, v = -\frac{\partial \psi}{\partial x}, u = cx^n f'(\eta), v = -\left(\frac{c\nu(n+1)}{2}\right)^{\frac{1}{2}} x^{\frac{n+1}{2}} \left(f(\eta) + \frac{n-1}{n+1} \eta f'(\eta)\right)$$

Here η is the similarity variable. ψ is stream function. $c(c > 0)$ is a parameter related to the surface stretching speed, n is the power index related to the surface stretching speed.

Introducing these variables in the equations we get the following dimensionless forms of the equations:

$$\left(1 + \frac{1}{\beta}\right) f''' + f f'' + \frac{2n}{n+1} f'^2 + d_1 \theta + d_2 \phi - (M + (1/K_1)) f' - Fs (f')^2 = 0, \quad (7)$$

$$\frac{1}{Pr} \theta'' + f \theta' + \left(1 + \frac{1}{\beta}\right) Ec f''^2 = 0, \quad (8)$$

$$\frac{1}{Sc} \phi'' + f \phi' + Sr \theta'' = 0, \quad (9)$$

with parameters:

$$\left. \begin{aligned} M &= \frac{2\sigma B_0^2}{\rho c}, K_1 = \frac{Kcx^{n-1}}{2\nu}, Fs = \frac{2bx}{\sqrt{K}}, Pr = \frac{\nu}{\alpha} = \frac{\rho\nu C_p}{k} = \frac{\mu C_p}{k}, \\ Gr_T &= \frac{2g\beta_T(T_w - T_\infty)}{(n+1)c^2 x^{2n-1}}, Gr_C = \frac{2g\beta_C(C_w - C_\infty)}{(n+1)c^2 x^{2n-1}}, u = cx^n \\ Ec &= \frac{u^2}{C_p(T_w - T_\infty)} = \frac{c^2 x^{2n}}{C_p(T_w - T_\infty)}, \nu = \frac{\mu}{\rho}, \\ Sc &= \frac{\nu}{D_m}, Du = \frac{D_m K_T (C_w - C_\infty)}{\nu C_S C_P (T_w - T_\infty)}, Sr = \frac{D_m K_T (T_w - T_\infty)}{\nu T_\infty (C_w - C_\infty)}. \end{aligned} \right\} \quad (10)$$

Here M is magnetic parameter(Hartmann number); K1 is Permeability parameter; Fs is Forchheimer parameter; Pr is Prandtl number; Gr_T is thermal Grashof number; Gr_C is concentration Grashof number; Ec is Eckert number; Du is Dufour number; Sc is Schmidt number ;and Sr is Soret number. And corresponding boundary conditions are as follow:

$$\begin{aligned} f(0) &= 0, f'(0) = 1 + \delta \left(1 + \frac{1}{\beta}\right) f''(0), \theta'(0) = -\gamma_1 [1 + \theta(0)], \phi'(0) = -\gamma_2 [1 + \phi(0)] \\ f'(\infty) &= 0, \theta(\infty) = 0, \phi(\infty) = 0 \end{aligned} \quad (11)$$

Where

$$N = N_1 x^{\frac{n-1}{2}}, \delta = N \left(\frac{(n+1)c\nu}{2} \right)^{\frac{1}{2}}, h_T = h_{T0} c x^{\frac{n-1}{2}}, \gamma_1 = h_{T0} \left(\frac{2\nu}{c(n+1)} \right)^{\frac{1}{2}} \quad (12)$$

$$h_C = h_{C0} c x^{\frac{n-1}{2}}, \gamma_1 = h_{C0} \left(\frac{2\nu}{c(n+1)} \right)^{\frac{1}{2}}$$

δ is called velocity slip parameter, γ_1 is called thermal slip parameter, and γ_2 is called concentration slip parameter.

The physical quantities of Engineering interest are the Skin-friction coefficient (rate of shear stress), the couple stress coefficient at the sheet, the local Nusselt number (rate of heat transfer), and the local Sherwood number (rate of mass transfer).

The local Skin-friction C_f , local Nusselt Number Nu_x and local Sherwood Number Sh_x are defined as follow:

$$C_f = \frac{\tau_w}{\frac{\rho U_w^2}{2}} = \frac{\mu_B \left(1 + \frac{1}{\beta} \right) \left(\frac{\partial u}{\partial y} \right)_{y=0}}{\frac{\rho U_w^2}{2}} \Rightarrow C_f = \left(\frac{2\nu(n+1)}{c} \right)^{\frac{1}{2}} x^{\frac{-(n+1)}{2}} f''(0),$$

$$C_f = \left(\frac{2(n+1)}{\text{Re}} \right)^{\frac{1}{2}} \left(1 + \frac{1}{\beta} \right) f''(0), \text{Re} = \frac{cx^{(n+1)}}{\nu} \quad (13)$$

$$Nu = - \frac{x \left(\frac{\partial T}{\partial y} \right)_{y=0}}{T_w - T_\infty} = - \left(\frac{c(n+1)}{2\nu} \right)^{\frac{1}{2}} x^{\frac{(n+1)}{2}} \theta'(0),$$

$$Nu = - \left(\frac{(n+1)cx^{(n+1)}}{2\nu} \right)^{\frac{1}{2}} \theta'(0) = - \left(\frac{(n+1)}{2} \text{Re} \right)^{\frac{1}{2}} \theta'(0). \quad (14)$$

Here $-\left(\frac{\partial T}{\partial y} \right)_{y=0}$ is a heat flux from the surface of the sheet.

$$Sh = - \frac{x \left(\frac{\partial C}{\partial y} \right)_{y=0}}{C_w - C_\infty} = - \left(\frac{c(n+1)}{2\nu} \right)^{\frac{1}{2}} x^{\frac{(n+1)}{2}} \phi'(0),$$

$$Sh = - \left(\frac{(n+1)cx^{(n+1)}}{2\nu} \right)^{\frac{1}{2}} \phi'(0) = - \left(\frac{(n+1)}{2} \text{Re} \right)^{\frac{1}{2}} \phi'(0). \quad (15)$$

Here $-\left(\frac{\partial C}{\partial y}\right)_{y=0}$ is a mass flow rate from the surface of the sheet and Re is the local Reynold Number.

3. METHOD OF NUMERICAL SOLUTION

The numerical solutions are obtained using the equations (7)-(9) and boundary conditions (11) for some values of the governing parameters, namely, the magnetic parameter M , Soret number Sr , Dufour number Du , Casson fluid parameter β , Prandtl number Pr , Schmidt number Sc , Eckert number Ec . Effects of M , Sr , Du , β , Pr , Sc , Ec on the steady boundary layer flow are discussed in detail. The numerical computation is done using the MATLAB in-built numerical solver `bvp4c`. In the computation we have taken $\eta_\infty = 10$ and axis according to the clear figure-visibility.

4. RESULT ANALYSIS AND DISCUSSION

In order to analyze the behaviour of non-dimensional linear velocity $f'(\eta)$, temperature $\theta(\eta)$, and concentration $\phi(\eta)$ profiles of the physical problem, numerical calculations are carried out for various values of magnetic parameter M , Soret number Sr , Dufour number Du , Casson fluid parameter β , Prandtl number Pr , Schmidt number Sc , and Eckert number Ec . Also, the Skin-friction factor and local Nusselt and local Sherwood numbers are discussed. For illustration of the results, the numerical data are tabulated in Tables 1-8 and plotted in Figs. 2-26.

For the convenience in calculation in Matlab following symbols are used for respective symbols used in modelling equations and boundary conditions:

$$a1 = f''(0), a2 = \theta'(0), a3 = \phi'(0), d = \delta, d1 = Gr_T, d2 = Gr_C, b = \beta, m1 = \gamma_1, m2 = \gamma_2, n1 = n.$$

The results for Skin-friction and local Nusselt number are compared with the previous published results, and are shown in Tables 1-2. It is observed that the obtained results are in good agreement with the published results.

Tables 1 and 2 present the values of Skin-friction coefficient and local Nusselt number for different

values of nonlinear stretching parameter $n1$ and Prandtl number Pr , respectively. The present results are compared with the results of Cortell [18] and Ullah et al. [17]. It is also observed from Table 1 that magnitude of Skin-friction coefficient $\left(1 + \frac{1}{\beta}\right) f''(0)$, increases with the increase in $n1$ whereas local Nusselt number decreases with the increase in $n1$ and increases with increase in Pr (Table 2).

Figs. 2-26 are plotted to study the effects of various parameters ($b, n1, M, Da, Fs, d, d1, d2, m1, m2, a1, a2, a3, Pr, Sc, Ec, Du$ and Sr) on the dimensionless velocity, temperature and concentration profiles.

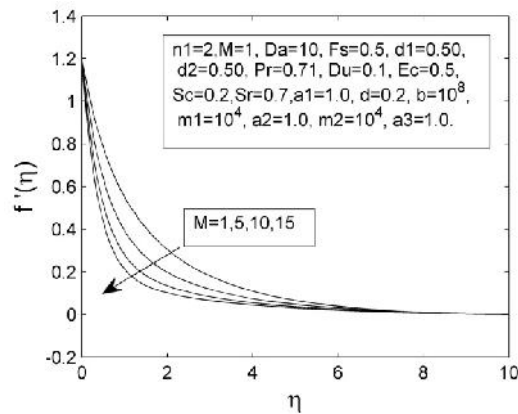


Fig. 2. Velocity profile $f'(\eta)$ with respect to similarity transformation η for some values of Magnetic parameter M

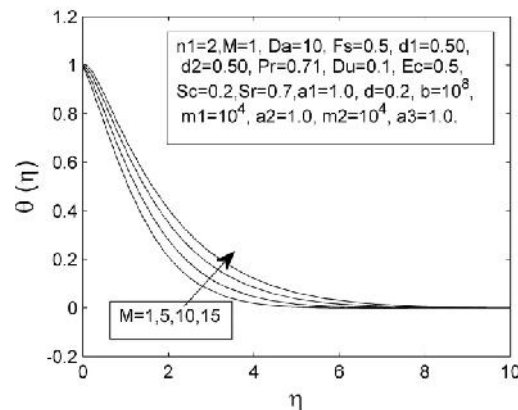


Fig. 3. Temperature profile $\theta(\eta)$ with respect to similarity transformation η for some values of Magnetic parameter M

The effect of M is illustrated in Fig. 2. All the trajectories are of same family with the magnetic number in between 1 and 15. It is seen that fluid velocity reduces as M increases. It is due to the fact that drag force, also known as Lorentz force is produced when magnetic field is applied to the fluid. This force has the tendency to slow down the velocity of the fluid in the boundary layer region. The decreasing pattern of velocity field with the increase in similarity variable shows that transverse magnetic field opposes the transport phenomenon. Thus the momentum boundary layer thickness decreases as M increases.

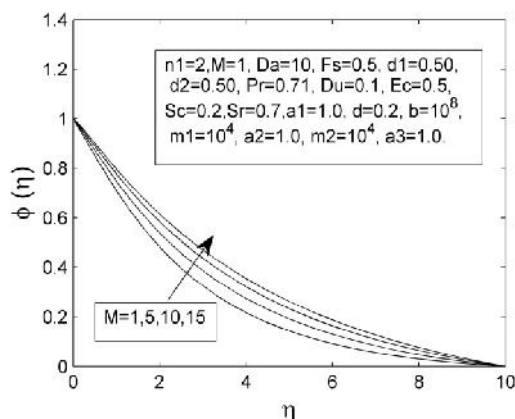


Fig. 4. Concentration profile $\phi(\eta)$ with respect to similarity transformation η for some values of Magnetic parameter M

Fig. 3 shows the behaviour of temperature profile for increasing values of Magnetic parameter M . The increasing values of M increase the fluid temperature as well as thermal boundary layer thickness. It is also observed that higher values of M increase the fluid temperature significantly and boundary layer

expands away from the wall. The explanation of this phenomenon is that the increasing M leads to a increase in thermal diffusion and results in thickening of boundary layer region.

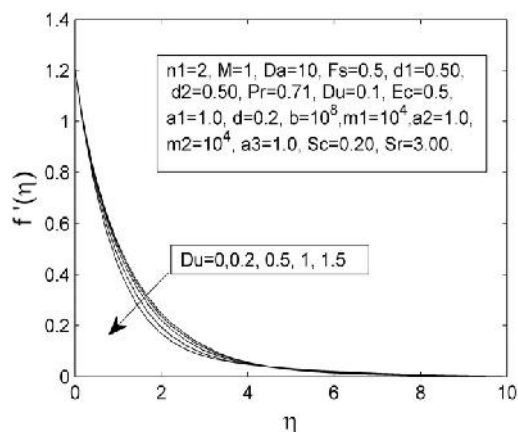


Fig. 5. Velocity profile $f'(\eta)$ with respect to similarity transformation η for some values of Dufour parameter Du

Fig. 4 shows the behaviour of concentration profile for increasing values of Magnetic parameter M . The increasing values of M increase the fluid concentration as well as concentration boundary layer thickness. It is also observed that higher values of M increase the fluid concentration significantly and boundary layer expands away from the wall. The explanation of this phenomenon is that the increasing M leads to a increase in concentration diffusion and results in thickening boundary layer. Thus, the increasing values of M increase the fluid concentration as well as concentration boundary layer thickness.

Table 1. Comparison of $-f''(0)$ for different values of $n1$ with $Fs=0.0$, $d1=0.0$, $d2=0.0$, $d=0.0$, $m1=10^4$, $m2=10^4$, $M=0$, $Pr=1.00$, $Du=0.0$, $Sc=0.22$, $a1=0.0$, $a2=1.0$, $a3=1.0$, $b=10^8$, $Ec=0.0$, $Da=10^7$, $Sr=0$

n1	$-f''(0)$		
	Cortell [18]	Ullah et al. [17]	Present
0.0	0.627547	0.6276	0.627631963479766
0.2	0.766758	0.7668	0.766906263551595
0.5	0.889477	0.8896	0.889594172073448
1	1.0	1.0	1.000062567556568
3	1.148588	1.1486	1.148660394543063
10	1.234875	1.2349	1.234952969673218
100	1.276768	1.2768	1.276830449563257

Table 2. Comparison of local Nusselt number $-\theta'(0)$ for various values of Pr and n1 with $Fs=0.0, d1=0.0, d2=0.0, d=0.0, m1=10^4, m2=10^4, M=0, Pr=1.00, Du=0.0, Sc=0.22, a1=0.0, a2=1.0, a3=1.0, b=10^8, Ec=0.0, Da=10^7, Sr=0$

$-\theta'(0), Pr=1,$			
n1	Cortell [18]	Ullah et al. [17]	Present
0.2	0.610262	0.6102	0.610277445039946
0.5	0.595277	0.5949	0.595283487517005
1.5	0.574537	0.5747	0.574829838650739
3.0	0.564472	0.5647	0.564775152915357

The effect of Dufour parameter is illustrated in Fig. 5. It is seen that fluid velocity profile reduces as Du increases and causes thinning of the corresponding boundary layer.

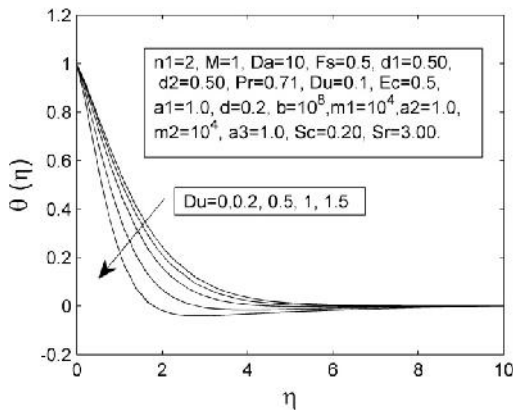


Fig. 6. Temperature profile $\theta(\eta)$ with respect to similarity transformation η for some values of Dufour parameter Du

It is shown in Fig. 6 that the temperature profile decreases with the increase in Dufour parameter and causes thinning of the corresponding boundary layer.

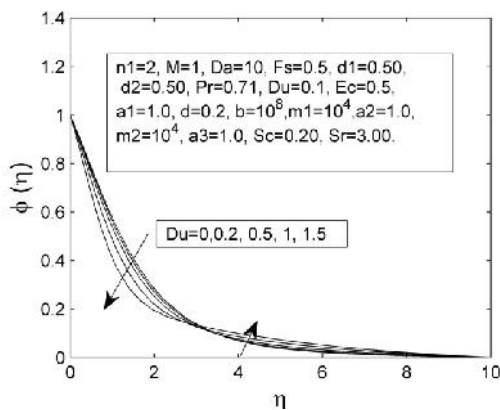


Fig. 7. Concentration profile $\phi(\eta)$ with respect to similarity transformation η for some values of Dufour parameter Du

It is shown in Fig. 7 that with the variation in the value of Dufour number Du, the concentration profiles show presence of point of intersection at some value of similarity variable in its (similarity variable's) range. Before the point of intersection concentration profiles decrease and after the point of intersection concentration profiles increase with the increase in Du and thus causes thinning before the point of intersection and thickening after the point of intersection of the corresponding boundary layers.

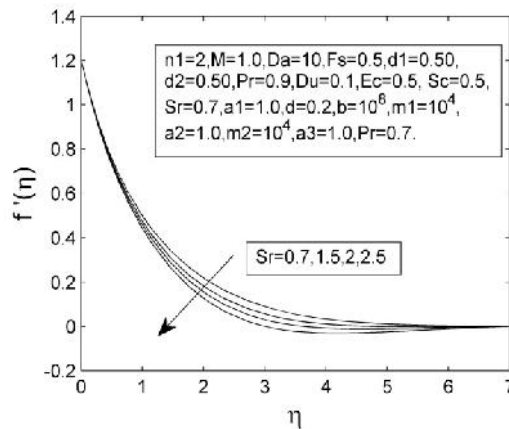


Fig. 8. Velocity profile $f'(\eta)$ with respect to similarity transformation η for some values of Soret parameter Sr

It is seen in Fig. 8 that velocity profile decreases with increasing Soret number and causes thinning of the corresponding boundary layer.

It is seen in Fig. 9 that the temperature profile increases with increasing Soret number and causes thickening of the corresponding boundary layer.

It is seen in Fig. 10 that the concentration profile decreases with increasing Soret number and causes thinning of the corresponding boundary layer.

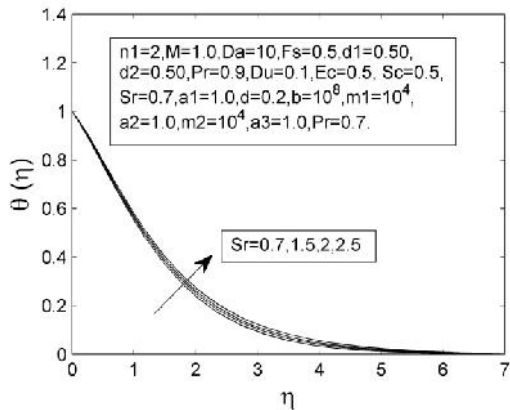


Fig. 9. Temperature profile $\theta(\eta)$ with respect to similarity transformation η for some values of Soret parameter Sr

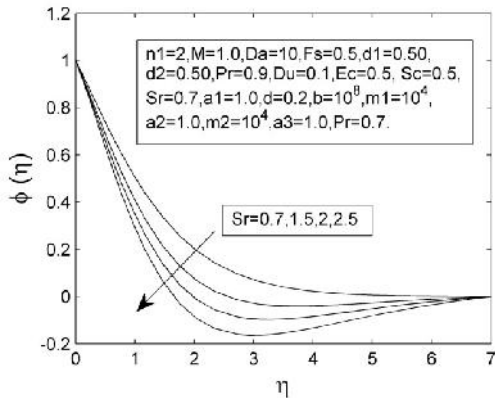


Fig. 10. Concentration profile $\phi(\eta)$ with respect to similarity transformation η for some values of Soret parameter Sr

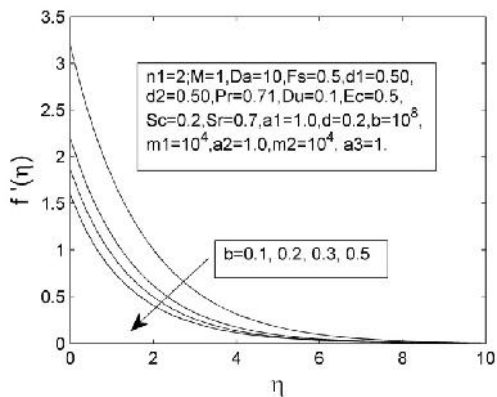


Fig. 11. Velocity profile $f'(\eta)$ with respect to similarity transformation η for some values of Casson parameter b

It is observed from Fig. 11 above that velocity profile decreases with the increase in Casson parameter b . physically, with increase in b , the fluid becomes more viscous and in result the fluid velocity reduces. Also, the momentum boundary layer thickness decreases as b increases. Further, as $b \rightarrow \infty$ the present phenomenon reduces to Newtonian fluid.

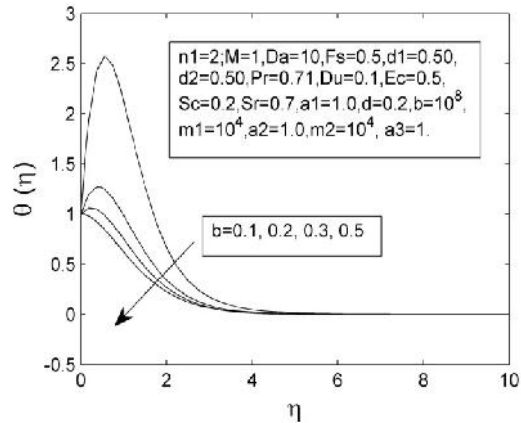


Fig. 12. Temperature profile $\theta(\eta)$ with respect to similarity transformation η for some values of Casson parameter b

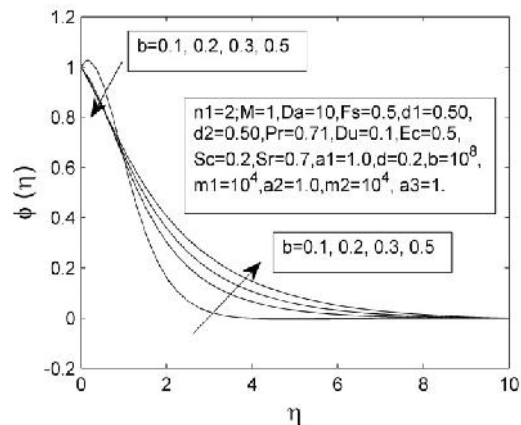


Fig. 13. Concentration profile $\phi(\eta)$ with respect to similarity transformation η for some values of Casson parameter b

It is observed from Fig. 12 that with the increase in the value of Casson parameter b , temperature profiles decrease. Also each curve shows having maxima and point of inflexion at some points in the range of similarity variable. And it causes thinning of the corresponding boundary layer before the point of inflexion.

It is observed from Fig. 13 that with the variation in the value of Casson parameter b , the concentration profiles shows presence of point of inflexion at some values of the similarity variable in its (similarity variable's) range. Before the point of inflexion concentration profile decreases and after the point of inflexion concentration profile increases with the increase in Casson parameter and thus causes thinning before the point of inflexion and thickening after the point of inflexion of the corresponding boundary layer.

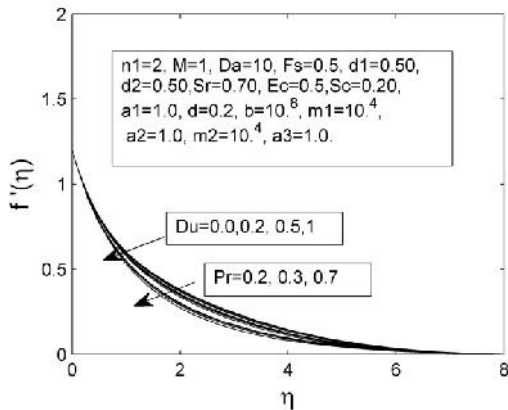


Fig. 14. Velocity profile $f'(\eta)$ with respect to similarity transformation η for some values of Dufour parameter Du and Prandtl number Pr

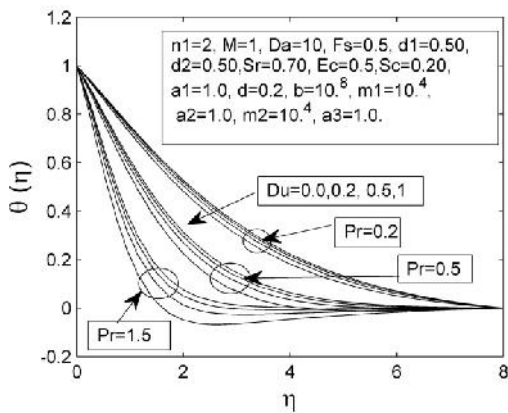


Fig. 15. Temperature profile $\theta(\eta)$ with respect to similarity transformation η for some values of Dufour parameter Du and Prandtl number Pr

It is observed from Fig. 14 that velocity profiles decrease with the increase in Dufour parameter Du and Prandtl number Pr and thus cause thinning of the corresponding boundary layers.

It is observed from Fig. 15 that temperature profiles decrease with the increase in Dufour parameter Du and Prandtl number Pr and thus cause thinning of the corresponding boundary layers.

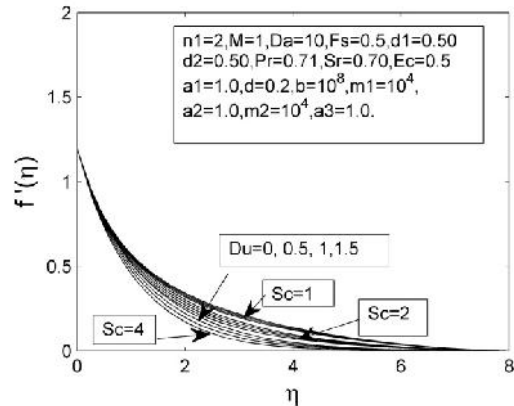


Fig. 16. Velocity profile $f'(\eta)$ with respect to similarity transformation η for some values of Dufour parameter Du and Schmidt number Sc

It is observed from Fig. 16 that velocity profiles decrease with the increase in Dufour parameter Du and Schmidt number Sc and thus cause thinning of the corresponding boundary layers.

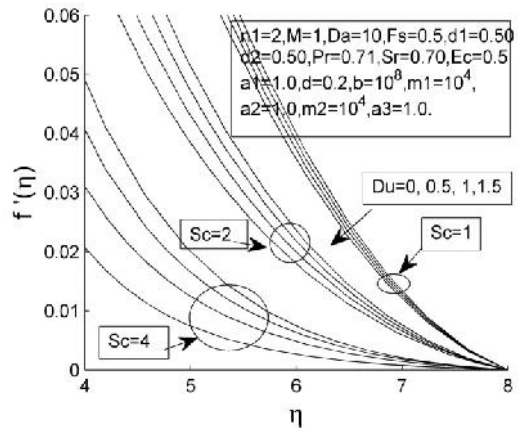


Fig. 17. Velocity profile $f'(\eta)$ with respect to similarity transformation η for some values of Dufour parameter Du and Schmidt number Sc

It is observed from Fig. 17 that velocity profiles decrease with the increase in Dufour parameter Du and Schmidt number Sc and thus cause thinning of the corresponding boundary layers.

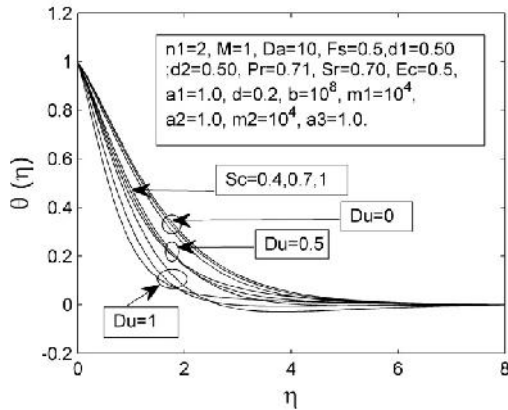


Fig. 18. Temperature profile $\theta(\eta)$ with respect to similarity transformation η for some values of Dufour parameter Du and Schmidt number Sc

It is shown in Fig. 18 that with the variation in the value of Dufour parameter Du and Schmidt number Sc , the temperature profiles show presence of point of intersection at some value of similarity variable in its (similarity variable's) range. Before the point of intersection temperature profiles decrease and after the point of intersection temperature profiles increase with the increase in Dufour parameter Du and Schmidt number Sc , and thus causes thinning before the point of intersection and thickening after the point of intersection of the corresponding boundary layers.

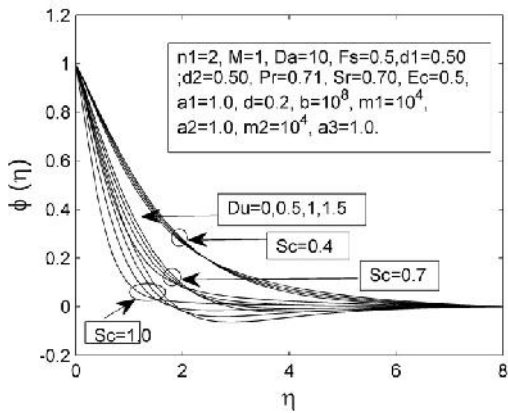


Fig. 19. Concentration profile $\phi(\eta)$ with respect to similarity transformation η for some values of Dufour parameter Du and Schmidt parameter Sc

It is shown in Fig. 19 that with the variation in the value of Dufour parameter Du and Schmidt number Sc , the concentration profiles show

presence of point of intersection at some value of similarity variable in its (similarity variable's) range. Before the point of intersection concentration profiles decrease and after the point of intersection concentration profiles increase with the increase in Dufour parameter Du and Schmidt number Sc , and thus causes thinning before the point of intersection and thickening after the point of intersection of the corresponding boundary layers.

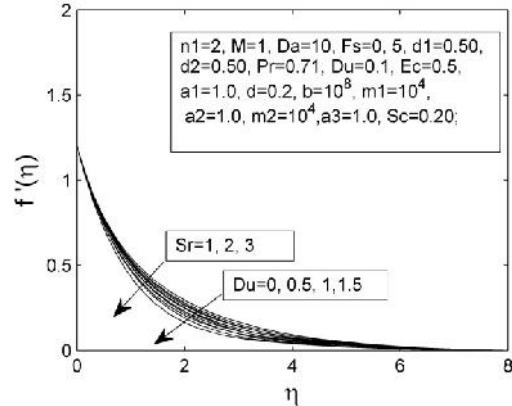


Fig. 20. Velocity profile $f'(\eta)$ with respect to similarity transformation η for some values of Dufour parameter and Soret parameter Sr

It is observed from Fig. 20 that velocity profiles decrease with the increase in Dufour parameter Du and Soret parameter Sr and thus cause thinning of the corresponding boundary layers.

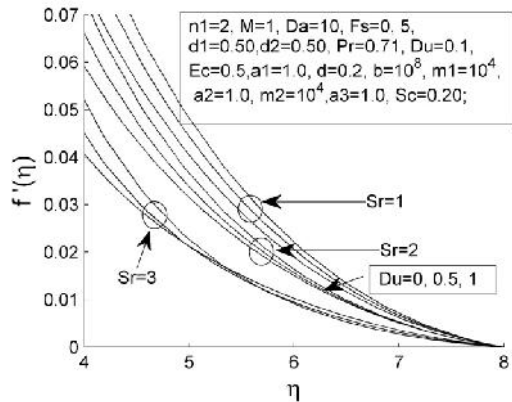


Fig. 21. Velocity profile $f'(\eta)$ with respect to similarity transformation η for some values of Dufour parameter and Soret parameter Sr

It is observed from Fig. 21 that velocity profiles decrease with the increase in Dufour parameter Du and Soret parameter Sr and thus cause thinning of the corresponding boundary layers.

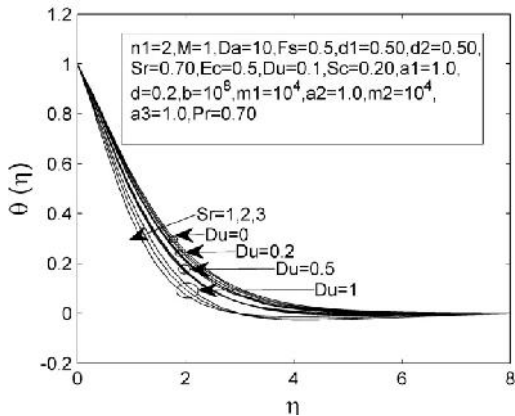


Fig. 22. Temperature profile $\theta(\eta)$ with respect to similarity transformation η for some values of Dufour parameter Du and Soret parameter Sr

It is shown in Fig. 22 that with the variation in the value of Dufour parameter Du and Soret parameter Sr , the temperature profiles show presence of point of intersection at some value of similarity variable in its (similarity variable's) range. Before the point of intersection temperature profiles decrease and after the point of intersection temperature profiles increase with the increase in Dufour parameter Du and Soret parameter Sr , and thus causes thinning before the point of intersection and thickening after the point of intersection of the corresponding boundary layers.

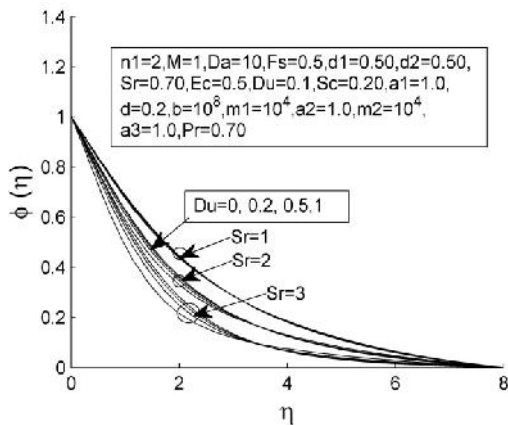


Fig. 23. Concentration profile $\phi(\eta)$ with respect to similarity transformation η for some values of Dufour parameter Du and Soret parameter Sr

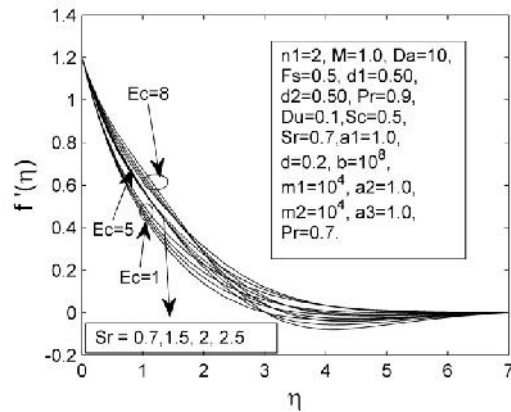


Fig. 24. Velocity profile $f'(\eta)$ with respect to similarity transformation η for some values of Soret parameter Sr and Eckert parameter Ec

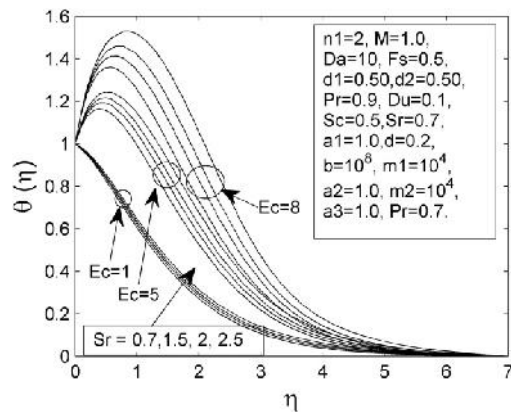


Fig. 25. Temperature profile $\theta(\eta)$ with respect to similarity transformation η for some values of Soret parameter Sr and Eckert parameter Ec

It is shown in Fig. 23 that with the variation in the value of Dufour parameter Du and Soret parameter Sr , the concentration profiles show presence of point of intersection at some value of similarity variable in its (similarity variable's) range. Before the point of intersection concentration profiles decrease and after the point of intersection concentration profiles increase with the increase in Dufour parameter Du and Soret parameter Sr , and thus causes thinning before the point of intersection and thickening after the point of intersection of the corresponding boundary layers.

It is observed from Fig. 24 that velocity profile decreases with the increase in Soret parameter Sr , thus cause thinning of the corresponding boundary layer an increases with the increase Eckert number Ec thus cause thickening of the corresponding boundary layer.

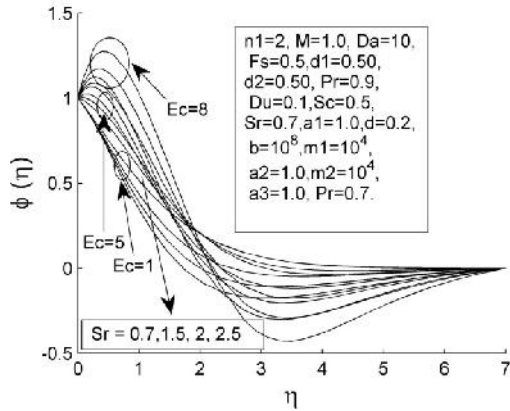


Fig. 26. Concentration profile $\phi(\eta)$ with respect to similarity transformation η for some values of Soret parameter Sr and Eckert parameter Ec

It is observed from Fig. 25 that with the variation in the value of Soret parameter Sr , and Eckert number Ec , each of the temperature profiles shows maxima and point of inflexion in the range

of similarity variable. With the each value of Soret parameter Sr , and Eckert number Ec , each curve shows having maxima before the point of inflexion. Also with the increase in the value of Soret parameter and Eckert number, temperature profiles show increase and thus cause increase in the corresponding boundary layer thickness.

It is observed from Fig. 26 that with the variation in the value of Soret parameter Sr , and Eckert number Ec , each of the concentration profiles shows maxima and point of inflexion in the range of similarity variable. With each value of Soret parameter Sr , and Eckert number Ec , each curve shows having maxima before the point of inflexion. Also with the increase in the value of Soret parameter Sr and Eckert number, concentration profiles show increase before the point of inflexion, and hence cause increase before the point of inflexion and decrease after the point of inflexion in the corresponding boundary layer thickness.

Table 3 shows with the increase in Magnetic parameter Skin-friction, local Nusselt number and local Sherwood number decreases.

Table 4 shows with the increase in Casson parameter Skin-friction, local Nusselt number and local Sherwood number increases.

Table 3. Comparison of Skin-friction $f''(0)$, local Nusselt number $-\theta'(0)$, and local Sherwood number $-\phi'(0)$ for various values of Magnetic parameter M

$n1=2; M=1; Da=10; Fs=0.5; d1=0.50; d2=0.50; Pr=0.71; Du=0.1; Ec=0.5; Sc=0.2; Sr=0.7; a1=1.0; d=0.2; b=10^8; m1=10^4; a2=1.0; m2=10^4; a3=1.0.$			
M	$f''(0)$	$-\theta'(0)$	$-\phi'(0)$
1	-1.139886286400067	0.414856222735359	0.291371985956979
5	-1.707705031432430	0.240533363861078	0.236481214248188
10	-2.264381188870255	0.063274575662640	0.189093904953875
15	-2.724242857459311	-0.081367644844538	0.154636326522287

Table 4. Comparison of Skin-friction $f''(0)$, local Nusselt number $-\theta'(0)$, and local Sherwood number $-\phi'(0)$ for various values of Casson parameter b

$n1=2; M=1; Da=10; Fs=0.5; d1=0.50; d2=0.50; Pr=0.70; Du=0.1; Ec=0.5; Sc=0.2; Sr=0.7; a1=1.0; d=0.2; b=10^8; m1=10^4; a2=1.0; m2=10^4; a3=1.0.$			
b	$f''(0)$	$-\theta'(0)$	$-\phi'(0)$
0.1	-1.938133150664395	-6.295211331613203	-0.320484926788943
0.2	-1.473378060541108	-1.442823157565096	0.183465539708107
0.3	-1.324805467549381	-0.534950892963336	0.257221030686203
0.5	-1.214615842077180	-0.025337735376427	0.287249701545771

Table 5 shows with the increase in Darcy parameter Skin-friction, local Nusselt number and local Sherwood number increases.

Table 7 shows with the increase in Prandtl number Skin-friction decreases and local Nusselt number and local Sherwood number increases.

Table 6 shows with the increase in Forchheimer parameter Skin-friction, local Nusselt number and local Sherwood number decreases.

Table 8 shows with the increase in Eckert number Skin-friction increases and local Nusselt number and local Sherwood number decrease.

Table 5. Comparison of Skin-friction $f''(0)$, local Nusselt number $-\theta'(0)$, and local Sherwood number $-\phi'(0)$ for various values of Darcy parameter Da

n1=2;M=1;Da=10;Fs=0.5;d1=0.50;d2=0.50;Pr=0.71;Du=0.1;Ec=0.5;Sc=0.2;Sr=0.7; a1=1.0;d=0.2;b=10 ⁸ ;m1=10 ⁴ ;a2=1.0;m2=10 ⁴ ;a3=1.0.			
Da	$f''(0)$	$-\theta'(0)$	$-\phi'(0)$
0.5	-1.428193623699829	0.328040454192572	0.262762395741959
1	-1.281374388721462	0.372846473212556	0.277173948582174
2	-1.203957866571336	0.395996971875209	0.284911124661897
3	-1.177501050005703	0.403819967527664	0.287573408826969

Table 6. Comparison of Skin-friction $f''(0)$, local Nusselt number $-\theta'(0)$, and local Sherwood number $-\phi'(0)$ for various values of Forchheimer parameter Fs

n1=2;M=1;Da=10;Fs=0.5;d1=0.50;d2=0.50;Pr=0.71;Du=0.1;Ec=0.5;Sc=0.2;Sr=0.7; a1=1.0;d=0.2;b=10 ⁸ ;m1=10 ⁴ ;a2=1.0;m2=10 ⁴ ;a3=1.0.			
Fs	$f''(0)$	$-\theta'(0)$	$-\phi'(0)$
0.5	-1.139886286400067	0.414856222735359	0.291371985956979
1	-1.208612809561646	0.401628776298048	0.287495526076845
2	-1.338383349016651	0.376015619156389	0.280167649510050
3	-1.459425519349771	0.351486715493245	0.273342292473521

Table 7. Comparison of Skin-friction $f''(0)$, local Nusselt number $-\theta'(0)$, and local Sherwood number $-\phi'(0)$ for various values of Prandtl number Pr

n1=2;M=1;Da=10;Fs=0.5;d1=0.50;d2=0.50; Du=0.1;Ec=0.5;Sc=0.2;Sr=0.7; a1=1.0;d=0.2;b=10 ⁸ ;m1=10 ⁴ ;a2=1.0;m2=10 ⁴ ;a3=1.0.			
Pr	$f''(0)$	$-\theta'(0)$	$-\phi'(0)$
0.7	-1.139171110747207	0.412286376828377	0.291199312367934
1	-1.157231825306829	0.478869265424159	0.296181869262054
2	-1.191414911346804	0.611623320537683	0.308360091315121
3	-1.209804887356637	0.679960625037383	0.315203633463110

Table 8. Comparison of Skin-friction $f''(0)$, local Nusselt number $-\theta'(0)$, and local Sherwood number $-\phi'(0)$ for various values of Eckert number Ec

n1=2;M=1;Da=10;Fs=0.5;d1=0.50;d2=0.50;Pr=0.70;Du=0.1;Ec=0.5;Sc=0.2;Sr=0.7; a1=1.0;d=0.2;b=10 ⁸ ;m1=10 ⁴ ;a2=1.0;m2=10 ⁴ ;a3=1.0.			
Ec	$f''(0)$	$-\theta'(0)$	$-\phi'(0)$
0.1	-1.147988244422926	0.540232249116676	0.307582454320623
0.2	-1.145767434719725	0.507907740910780	0.303440467248767
0.3	-1.143558180413784	0.475809857492194	0.299329499846729
0.5	-1.139171110747207	0.412286376828377	0.291199312367934

Table 9. Comparison of Skin-friction $f''(0)$, local Nusselt number $-\theta'(0)$, and local Sherwood number $-\phi'(0)$ for various values of Dufour number Du

n1=2;M=1;Da=10;Fs=0.5;d1=0.50;d2=0.50;Pr=0.70;Du=0.1;Ec=0.5;Sc=0.2;Sr=0.7; a1=1.0;d=0.2;b=10 ⁸ ;m1=10 ⁴ ;a2=1.0;m2=10 ⁴ ;a3=1.0.			
Du	$f''(0)$	$-\theta'(0)$	$-\phi'(0)$
0	-1.139341254219237	0.400032497066902	0.296468803292375
0.2	-1.143544759569682	0.417496237457631	0.297833579239204
0.5	-1.150011965516246	0.444375863555847	0.299947517761085
1	-1.161253400554637	0.491133315364581	0.303662254401080

Table 10. Comparison of Skin-friction $f''(0)$, local Nusselt number $-\theta'(0)$, and local Sherwood number $-\phi'(0)$ for various values of Schmidt number Sc

n1=2;M=1;Da=10;Fs=0.5;d1=0.50;d2=0.50;Pr=0.71;Du=0.1;Ec=0.5;Sc=0.2;Sr=0.7; a1=1.0;d=0.2;b=10 ⁸ ;m1=10 ⁴ ;a2=1.0;m2=10 ⁴ ;a3=1.0.			
Sc	$f''(0)$	$-\theta'(0)$	$-\phi'(0)$
0.2	-1.139886286400067	0.414856222735359	0.291371985956979
0.4	-1.176935210977778	0.386151355496659	0.443770131850051
0.7	-1.215081398526230	0.360817373104762	0.628942510557584
1.2	-1.255405680773496	0.343770968980801	0.873476192982244

Table 11. Comparison of Skin-friction $f''(0)$, local Nusselt number $-\theta'(0)$, and local Sherwood number $-\phi'(0)$ for various values of Soret number Sr

n1=2;M=1;Da=10;Fs=0.5;d1=0.50;d2=0.50;Pr=0.70;Du=0.1;Ec=0.5;Sc=0.2;Sr=0.7; a1=1.0;d=0.2;b=10 ⁸ ;m1=10 ⁴ ;a2=1.0;m2=10 ⁴ ;a3=1.0.			
Sr	$f''(0)$	$-\theta'(0)$	$-\phi'(0)$
0.7	-1.143632365431753	0.405620505160762	0.302985470126012
1.5	-1.154724386800227	0.397577058525297	0.340314127119831
2	-1.161673814489628	0.392217170730794	0.362464009525076
2.5	-1.168628603664313	0.386577782183745	0.383611994611814

Table 9 above shows with the increase in Dufour number, Skin-friction decreases and local Nusselt number and local Sherwood number increase.

Table 10-11 above shows with the increase in Schmidt number and Soret parameter, Skin-friction, and local Nusselt number decrease and local Sherwood number increases.

5. CONCLUSION

In the present paper the numerical study of effects of Soret and Dufour and viscous dissipation parameters on steady magnetohydrodynamic Casson fluid flow through non-Darcy porous medium is explored. By suitable similarity transformations, the governing boundary layer equations are transformed to ordinary differential equations. The method, the

numerical computation with `bvp4c`, a MATLAB program, is applied to solve these equations. The effects of magnetic Parameter, Soret parameter, Dufour parameter, Prandtl number, Schmidt number, Eckert number, and Casson parameter on velocity, heat transfer, and concentration profiles, Skin- frictions, local Nusselt number and local Sherwood number are computed and discussed numerically and presented through tables and graphs.

From the above work following results are concluded.

Velocity profiles decrease and thus cause thinning of the corresponding boundary layers with the increase in Magnetic parameter, Dufour parameter, Soret parameter, Casson parameter, Prandtl number, and Schmidt number.

Temperature profiles decrease and thus cause thinning of the corresponding boundary layers with the increase in Dufour parameter, Casson parameter, Prandtl number, and Schmidt number.

Concentration profiles decrease and thus cause thinning of the corresponding boundary layers with the increase in Soret parameter, and Schmidt number.

Before the point of inflexion concentration profile decreases and after the point of inflexion concentration profile increases and thus causes thinning before the point of inflexion and thickening after the point of inflexion of the corresponding boundary layer, with the increase in Dufour parameter, and Casson parameter.

Velocity profiles increase and thus cause thickening of the corresponding boundary layers with the increase in Eckert number.

Temperature profiles increase and thus cause thickening of the corresponding boundary layers with the increase in magnetic parameter, Soret parameter, Eckert number.

Concentration profiles increase and thus cause thickening of the corresponding boundary layers with the increase in magnetic parameter.

Concentration profiles show increase before the point of inflexion and decrease after the point of inflexion, and hence cause increase before the point of inflexion and decrease after the point of inflexion in the corresponding boundary layer thickness, with the increase in the value of Soret parameter and Eckert number.

Skin-friction increases with the increase in Casson parameter, Darcy parameter, Prandtl number, and Dufour parameter.

Local Nusselt number increases with the increase in Casson parameter, Darcy parameter, Eckert number, Schmidt number, and Soret parameter.

Local Sherwood number increases with the increase in Casson parameter, Darcy parameter, Eckert number, Schmidt number.

Skin friction decreases with the increase in Magnetic parameter, Forchheimer parameter, Eckert number, Schmidt number, and Soret parameter.

Local Nusselt number decreases with the increase in Magnetic parameter, Forchheimer parameter, Prandtl number, and Dufour parameter.

Local Sherwood number decreases with the increase in Magnetic parameter, Forchheimer parameter, Prandtl number, Dufour parameter, Schmidt number, and Soret parameter.

COMPETING INTERESTS

Author has declared that no competing interests exist.

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